

# Development of a Unified Numerical Kinetic Approach, Taking into Account Many-Particle Interactions in Liquid-Vapor Systems

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**Abstract:** The study of evaporation and condensation should include consideration of heat and mass transfer processes inside the liquid, in the inter-phase transition domain, in the Knudsen layer, and in the outer area. Possible way to realize it is to use the conjugate approach, in which the description of these regions is carried out employing a single computational method. This method allows us to consider the condensed phase and gas as a single system and use the solution of kinetic equations throughout the region. Currently, processes in the gas phase have been studied quite well. The greatest obstacle to the use of kinetic equations in the condensed phase is the description of collisions involving multiple particles at the same time. In this paper a procedure is proposed to take the multi-particulate interactions within the condensed phase into account. Such approach is applied to the test study of the thermal conductivity problem for argon, neon, xenon, and krypton. Values of thermal conductivity coefficients for different quantities of interacting particles have been obtained. The comparison with corresponding experimental data is presented. Thus, the integral of paired collisions in the Boltzmann kinetic equation can be replaced by the proposed computational procedure. This approach provides a description of both liquid and gas at the level of the distribution function and ensures that the conditions at the interface are set correctly.

**Keywords:** Boltzmann Equation, Interface Phenomena, Joint Solution

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## 1. Introduction

It is well known at present that the proper investigation of nonequilibrium processes on a vapor-condensate interface can be made based on molecular kinetic theory (MKT). The primary function of this theory is the velocity distribution function (DF)  $f$  of molecules. In order to find this function, the Boltzmann kinetic equation (BKE) should be solved, which calls for the formulating boundary condition. These conditions require the knowledge of the DF for the molecules that escape from condensed matter. This DF is, as a rule, specified using various models (e.g., diffuse or mirror reflection). Less often, it is found experimentally or by setting the condensation or accommodation coefficients.

Few works have modeled liquid and gas phases within a single computational method [1-5]. Therefore, there is a need for a single framework that models both the liquid and vapor

phases. One of the features of the present problem is the presence of heat and mass transfer, as seen in both liquid and vapor. During this transfer, the processes in one phase can strongly influence the phenomena in the other. Generally, the heat falling to the surface is spent on heating, and the evaporation of the liquid. At this vapor formed as a result of this evaporation is removed from the surface. The formation of a vapor flux occurs in the layer near the vapor-liquid interface. The thickness of this layer is equal to several mean free paths of vapor molecules.

Thus, the study of evaporation should include consideration of heat and mass transfer processes inside the liquid, in the interphase transition layer, in the Knudsen layer, and in the outer area. One possible way includes using the conjugate approach, in which the description of the liquid phase, interphase layer, and Knudsen layer is carried out employing a single computational method. The development

of this approach was initiated by the authors in the paper [6]. In this paper, a model of the interaction of many particles in the condensed phase is proposed, which assumes that collisions are pair-wise independent.

The collision integral is the most complex portion of the kinetic equation, which should take into account the interaction in the condensed phase between several ( $M$ ) particles. According to the following research [7, 8], the correlations are maximal at  $M=3$  and decrease rapidly with growth  $M$  due to molecular chaos. Based on this fact, an approach that allows us to consider the multi-particle interaction as a set of paired collisions has been proposed [9].

This step can be considered the first approximation in the construction of a single, conjugate, end-to-end method. However, the role of correlations in the interaction of condensed matter particles among themselves is not fully understood at present. Therefore, for the further development of the conjugate approach, it is necessary to develop a new method in which the interacting particles will be considered as a single system. In this paper a version of such method is presented.

## 2. Description of the Method

### 2.1. Kinetic Equation for Liquid Phase

The presented paper proposes to solve the kinetic equation inside the condensed phase:

$$\frac{\partial f}{\partial t} + \xi \frac{\partial f}{\partial \mathbf{r}} = Z_M. \quad (1)$$

The direct numerical solution of this type kinetic equation

$$\mathbf{P} = \begin{bmatrix} p_1 \\ p_2 \\ p_3 \\ \dots \\ p_{N-2} \\ p_{N-1} \\ p_N \end{bmatrix} = \begin{bmatrix} \xi_{x1} \\ \xi_{y1} \\ \xi_{z1} \\ \dots \\ \xi_{xN} \\ \xi_{yN} \\ \xi_{zN} \end{bmatrix}, \quad |\mathbf{P}| = \sqrt{\xi_{x1}^2 + \xi_{y1}^2 + \xi_{z1}^2 + \dots + \xi_{xN}^2 + \xi_{yN}^2 + \xi_{zN}^2}. \quad (2)$$

Interaction between all  $M$  particles will lead to a change in the state of the system, which can be described by the new vector  $\mathbf{Q}$ . A transition of the system from one state to another as a result of the interaction of particles will be described by some operator  $\mathbf{F}$ :  $\mathbf{Q} = \mathbf{F}\mathbf{P}$ . The components of the vector  $\mathbf{Q}(q_1, q_2, \dots, q_j, \dots, q_N)$  will then be the velocities of the condensed phase particles after the interaction  $\xi'(\xi'_x, \xi'_y, \xi'_z)$ :

$$\mathbf{Q} = \begin{bmatrix} q_1 \\ q_2 \\ q_3 \\ \dots \\ q_{N-2} \\ q_{N-1} \\ q_N \end{bmatrix} = \begin{bmatrix} \xi'_{x1} \\ \xi'_{y1} \\ \xi'_{z1} \\ \dots \\ \xi'_{xN} \\ \xi'_{yN} \\ \xi'_{zN} \end{bmatrix}, \quad |\mathbf{Q}| = \sqrt{\xi'^2_{x1} + \xi'^2_{y1} + \xi'^2_{z1} + \dots + \xi'^2_{xN} + \xi'^2_{yN} + \xi'^2_{zN}}. \quad (3)$$

by the manner of [6, 9-11] is used.

Regarding the description of the condensed phase, the left side of equation (1) only describes the transfer of the distribution function and not the transformation of this function during the atom interactions. The value  $Z_M$  on the right side is an analog of the paired integral of collisions but is designed to take into account the simultaneous interaction of the  $M$  atoms (molecules) of the condensed phase. It describes collisions, provided that mass, momentum, and kinetic energy are preserved during the interaction, as well as the integral for paired collisions in the Boltzmann kinetic equation. In this work,  $Z_M$  is replaced by the computational procedure described below. This method allows the use of a single numerical algorithm to determine macro parameters inside both the vapor and the liquid.

### 2.2. Turn Method for Describing Multi-particle Interactions

At both low and room temperatures, it can be assumed that each liquid particle has three degrees of freedom associated with the translational motion in Cartesian space  $\mathbf{r}(x, y, z)$ . A group of  $M$  particles in the liquid is isolated, which were located in close proximity to each other. It is assumed that the moving particle has three degrees of freedom. Therefore, the system of  $M$  particles has  $N = 3M$  degrees of freedom. When passing through the equilibrium position of each particle, its velocity  $\xi(\xi_x, \xi_y, \xi_z)$  can be fixed. Further, when constructing the computational algorithm, we will assume that the components of vector  $\mathbf{P}(p_1, p_2, \dots, p_j, \dots, p_N)$  will comprise all of the velocities of atoms (molecules) before the interaction  $\xi(\xi_x, \xi_y, \xi_z)$ :



various temperatures. The heat flux in the direction  $x$  was defined as the third-order moment of the distribution function:

$$q_x = \frac{1}{2} m \int (\xi - u)^2 (\xi_x - u_x) f d\xi, \quad (6)$$

where  $d\xi = d\xi_x d\xi_y d\xi_z$ ,  $u(u_x, u_y, u_z)$  is the mean particle velocity vector,  $k$  is the Boltzmann constant,  $m$  is the mass of the molecule.

Then, thermal conductivity coefficients were calculated by the formula:

$$\lambda = q_x L / (T_1 - T_2). \quad (7)$$

To solve the problem of heat flow in the liquid, the Chapman-Enskog function [14] was taken as boundary conditions:

$$f_1 = f_M \left[ 1 - \frac{q_x}{p} \frac{c_x}{RT} \left( 1 - \frac{1}{5} \frac{c^2}{RT} \right) \right], \quad (8)$$

where  $f_M$  is the Maxwell distribution function calculated at temperature  $T = T_1$  or  $T = T_2$ , and density was determined from the condition of impermeability of surfaces;  $c_x = \xi_x - u_x$ ;  $c^2 = (\xi - u)^2$ ;  $p$  – pressure.

Substituting values  $q_x$  in formula (6), as well as boundary temperatures  $T_1$  or  $T_2$  and solving equations (1) with Chapman-Enskog functions as the boundary conditions, we will obtain values of heat flow and temperature difference. Initially, they may not coincide with those substituted in (8). Therefore, an iterative process is needed until an agreement between  $T_1$ ,  $T_2$ , and  $q_x$  is reached in both the formula and the results. Next, the thermal conductivity coefficient in the liquid is determined in accordance with (7).

### 3.3. Results and Analysis

Examples of the results of the calculation of thermal conductivity coefficients for different substances are presented in Table 1.

Table 1. Thermal conductivity factors for Ar, Ne, Kr, and Xe.

$T_0$ , K	$M$	$\lambda \times 10^3$ , W/mK	$\lambda_{tabl} \times 10^3$ , W/mK	$T_0$ , K	$M$	$\lambda \times 10^3$ , W/mK	$\lambda_{tabl} \times 10^3$ , W/mK
Argon				Neon			
	3	134.1			3	145.7	
87. (p=0.1MPa)	4	116.4	130.	25. (p=0.05MPa)	4	126.5	117.
	5	93.57			5	101.7	
100. (p=1MPa)	4	124.8	110.9	27. (p=0.1MPa)	4	131.5	113.
	5	100.3			5	105.7	
120. (p=2MPa)	5	109.9	85.5	30. (p=0.22MPa)	5	111.4	92.
	6	75.38			6	81.53	
	5	114.4			2	28.95	
130. (p=3MPa)	6	78.46	73.6	103. (p=0.1MPa)	3	23.92	22.7
	7	62.77			4	20.14	
200. (p=0.1MPa)	2	13.84	12.6	198. (p=0.1MPa)	2	40.14	37.1
	3	10.81			3	33.16	
300. (p=0.1MPa)	2	16.95	17.7	273. (p=0.1MPa)	2	47.14	46.1
	3	13.24			3	38.94	
Krypton				Xenon			
	3	97.35			3	73.94	
125. (p=0.14MPa)	4	84.51	87.6	170. (p=0.13MPa)	4	64.21	64.0
	5	67.94			5	51.62	
	3	99.28			3	76.11	
130. (p=0.2MPa)	4	86.19	84.0	180. (p=0.22MPa)	4	66.07	65.5
	5	69.29			5	53.11	
180. (p=0.1MPa)	2	6.96	5.98	250. (p=0.1MPa)	2	4.96	4.76
	3	5.22			3	3.63	
300. (p=0.1MPa)	2	8.99	9.58	300 (p=0.1MPa)	2	5.44	5.69
	3	6.74			3	3.97	

The last columns of all tables contain values taken from reference literature [15].

It is important to note that the nonequilibrium Chapman-Enskog boundary functions for liquid and half- Maxwell functions at diffuse reflection scheme for gas were used for obtaining the data in the table.

As observed from the results obtained, the experimental data ( $\lambda_{tabl}$ ) are consistent with the calculation results at  $M = 3-5$  for liquids and at  $M = 2-3$  for gases with different densities. Table 1 also demonstrates that at high

enough pressures, the number of interacting argon particles tends to be 5 – 7. The quantity of particles able to interact at normal conditions for all gases  $M$  is close to 2.

The results presented were obtained for the length of the calculating region  $L \approx (300-500)d$ . Obviously, the temperature difference  $T_1/T_2 = 1.1$  is too large for such a thin liquid layer. Therefore, it was important to make calculations using the proposed approach for the lowest temperature ratio.

Figure 2 shows the dependence dimensionless heat flux on

$x$  at  $T_1/T_2 = 1.001$  and the number of interacting particles  $M = 4$ .

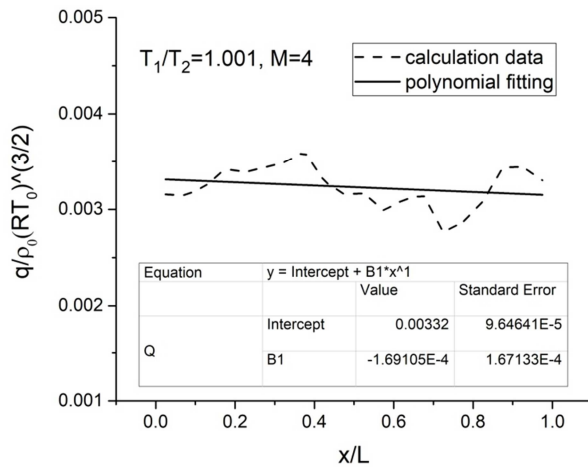


Figure 2. Dependence of heat flux density on  $x$  at a low temperature ratio.

for limiting surfaces.  $\rho_0$  is density at  $T_0$  and  $p$ ,  $R$  is individual gas constant, for large enough  $T_0$   $\rho_0 = \frac{p}{RT_0}$ .

The heat flux is shown by a dashed line. A solid line indicates the result of polynomial interpolation using Origin 9. Thus, the spread of the computed data is statistically processing, and the resulting solid line is physically correct.

Further reduction of the temperature ratio does not allow us to obtain adequate results. Thus,  $T_1/T_2 = 1.001$  is the limit for the proposed approach at this stage of the work.

## 4. Conclusion

An approach has been proposed to take the multi-particulate interactions within the condensed phase into account. At the first stage this approach was applied to the study of the thermal conductivity problem for argon, neon, xenon, and krypton. Values of thermal conductivity coefficients for different numbers of interacting particles were obtained. Satisfactory agreement was found with the experimental data at  $M = 3-5$  for liquid and  $M \approx 2$  for gases under normal conditions.

This approach is planned to apply in close future for evaporation-condensation problems solving without using of any empirical values concerning interface: accommodation coefficients and so on. In evaporation-condensation processes substance transfers from liquid (solid) to vapor. The velocity distribution functions of molecules for condensate and vapor can be obtain by suggested method as solution result. Then any macroscopic values such as density, temperature, mass, momentum, heat fluxes are determined as integrals of distribution functions in 3D velocity space.

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